



Seasonal Gasoline Volatility Classes
(Shipments from Origin)

Reid Vapor Pressure, D5191^{1/}

March 1 - September 15 DVPE using EPA formula^{2/}
September 16 – February 28 DVPE using D5191 formula

	Class AA	Class A	Class B	Class C	Class D	Class E
Distillation, ASTM D 86 ^{3/}						
10% Evaporated °F, max	158.0	158.0	149.0	140.0	131.0	122.0
50% Evaporated °F, min	150.0	150.0	150.0	150.0	150.0	150.0
50% Evaporated °F, max	250.0	250.0	245.0	240.0	235.0	230.0
90% Evaporated °F, max	374.0	374.0	374.0	365.0	365.0	365.0
Final Boiling Point °F, max ^{4/}	425.0	425.0	425.0	425.0	425.0	425.0
Residue, vol % max	2	2	2	2	2	2
Driveability Index, D4814, max ^{2/3/}	1250	1250	1240	1230	1220	1200

Pre Ethanol Blend

	<u>Class 1</u>	<u>Class 2</u>	<u>Class 3</u>	<u>Class 4</u>	<u>Class 5</u>
Vapor to Liquid Ratio=20:1, °F ^{5/} D5188, min	140	133	122	116	105
Vapor to Liquid Ratio=20:1, °F ^{5/} Area V only D5188, min	140	133	122	122	108

Post Ethanol Blend

	<u>Class 1</u>	<u>Class 2</u>	<u>Class 3</u>	<u>Class 4</u>	<u>Class 5</u>
Vapor to Liquid Ratio=20:1, °F ^{3/5/} D5188, min	129	122	116	107	102
Vapor to Liquid Ratio=20:1, °F ^{3/5/} Area V only D5188, min	129	122	116	116	105

- 1/ All gasoline deliveries will not exceed applicable Federal and State requirements.
- 2/ The calculation required for the EPA compliance period is published in part 1090.1355.
- 3/ Specifications shall be met after blending with 9 % to 10 % denatured fuel ethanol.
- 4/ The final boiling point of all gasoline deliveries at terminals will be at or below 437°F as determined by ASTM D86
- 5/ D5188 is the referee test method. The alternative equations in D4814 may also be used.